Chemical Biological Individual Protection Conference Charleston, South Carolina, 7-9 March 2006

Filtration Technology

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Past-Present-Future

1940s	1950-60		1980				2000-10
M11 Filter		M13 Filter		C2 F	Filter		JSGPM Filter
H-Capacity		Sorbent/HEPA		M-Ca	pacity		Primary CWA
H-dP		L-M Capacity		М	dP		Secondary TIC
H Weight		M dP		MW	eight		Packed Bed
H Profile		L weight		M Profile		L-M Capacity	
	L Profile				L-M dP		
						L-M Profile	
2010			2020 +				
	NGGPM Filter						
	Composite Beds			Non Sorbent			
	Interchar	ngeable Media			S	СВА	
		ngeable Media Spectrum Prot			S	СВА	
	Broad S	•			S	CBA	
	Broad S L-0	pectrum Prot			S	CBA	

Direction and Challenges

- Rapid Advancement In Sorbent Technology
- New Requirements
 - Increasing Number And Classes Of Chemicals
- Technical Challenges
 - Broad Spectrum Protection
 - Small Integrated Envelope
 - Lightweight And Acceptable Pressure Drop

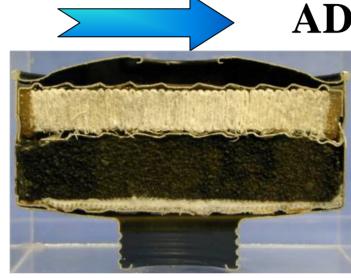
Direction and Challenges

- Current Filters Continue To Be Oriented To Granular Packed Bed.
- Community Moving Towards Broader Spectrum Protection With Lower Capacity Requirements.
- There Are Improved Filter Technology Solutions In The Form Of Supported Sorbent Structures And Particulate Media That Will Offer Lower Profile Filters With Broad Spectrum Protection Capabilities.

Filtration Principles

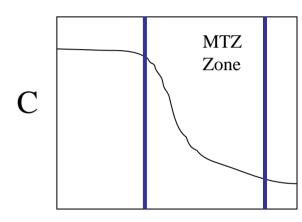
HEPA (Particulate)

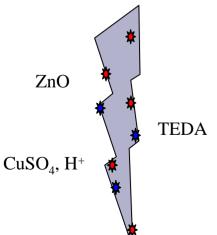
C2 CANISTER



ADSORBER

(Vapor)



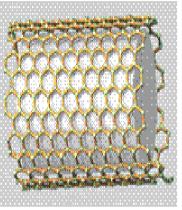


Adsorbent Requirements

⁰ Bed Depth

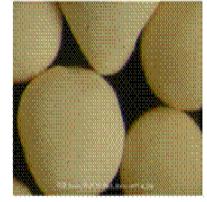
Microporosity for physical adsorption
 Pore distribution that can support reactants
 Basic sites for removal of acid gases
 Acid sites for removal of base-forming and basic gases
 Access to reactive sites when adsorbed water is present

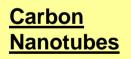
Adsorbents

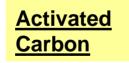












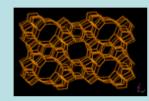




Sorbent Development

BF-38

- ZSM-5
 - MFI-type zeolite
 - Acidified



• Removes basic/base-forming TICs

- Ammonia
- Ethylene oxide

ARC





- Bituminous coal based activated carbon
- Impregnated w/ copper chloride

KRM-623

ZSM-5

 MFI-type zeolite
 Alkaline



 Removes fuming nitric acid, nitrogen dioxide

90/10 Blend

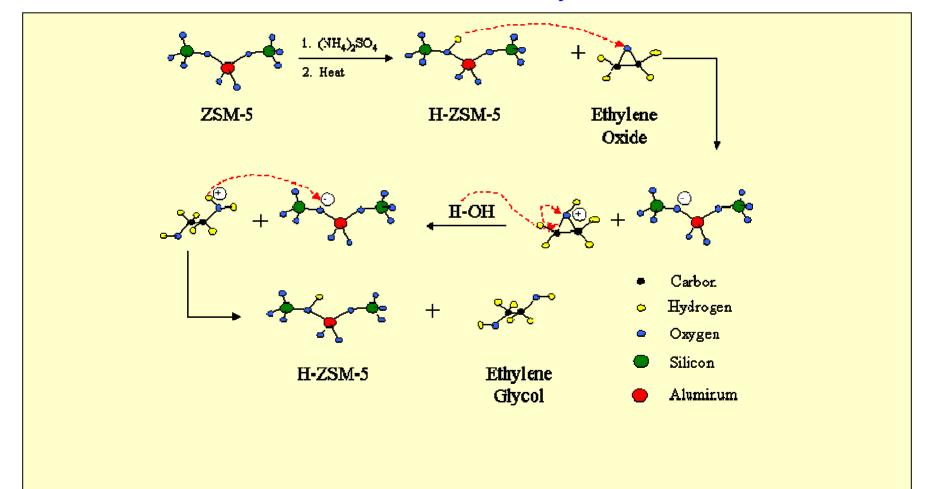


-10% acid chloride impregnated carbon

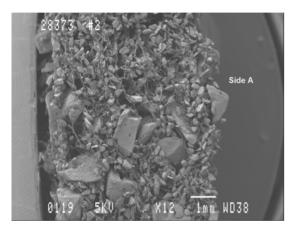
• Removes traditional CWAs + ammonia

Sorbent Development

SORBENT DEVELOPMENT EO Removal Mechanism by BF-38

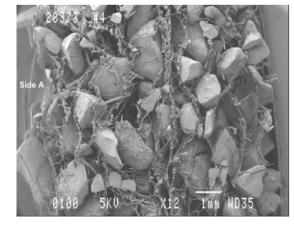


Advanced Adsorbent Supports



Description:

Flexible extruded web of elastomeric fibers loaded above traditional levels with broad range of treated carbon particles and with wide latitude in basis weight capability



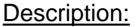
Advancement Over Fielded Systems:

- Lower pressure drop, power
- Lighter weight, less maintenance
- Broader spectrum of protection CWAs + TIC/TIMs

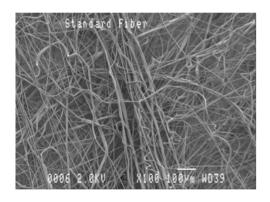
Source: 3M

Advanced Particulate Filtration

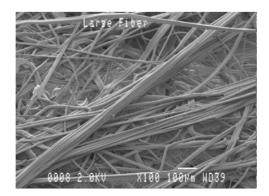
Electret Filter Media

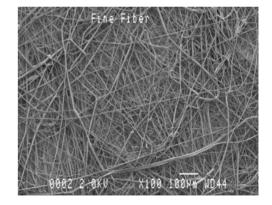


Multiple pleated layers of fiberglass, membranes, or electret webs combine to provide thermally stable non-clogging filters that are resistant to: wetting, oily mist, and Chem/Bio agents.



Large Fiber (20+ micron) Standard fiber (7-10 micron)





Fine Fiber (3-5 micron)

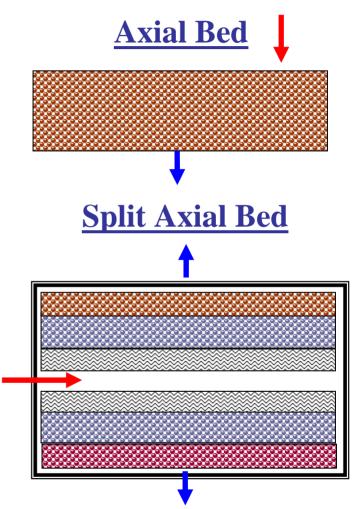
Source:3M

Filter Bed Design

Radial Bed

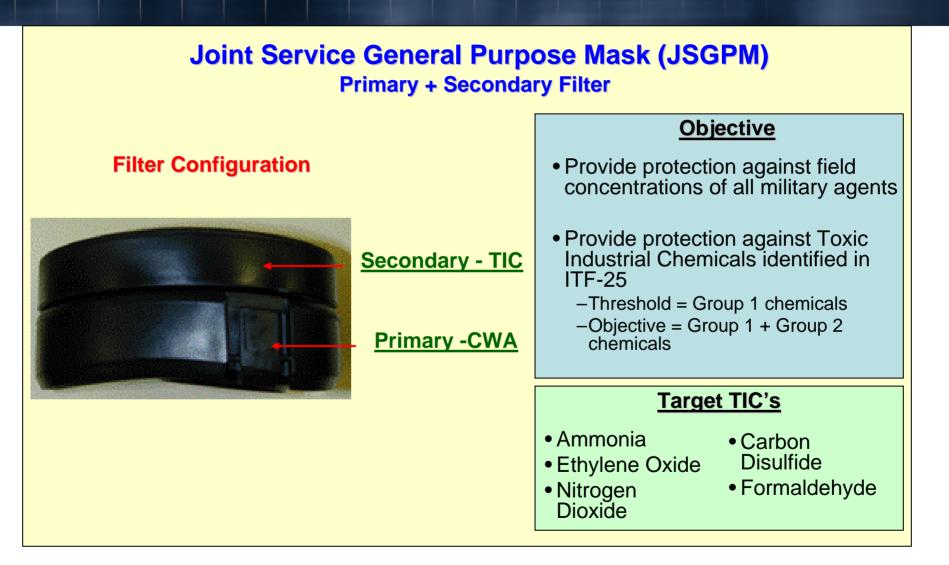


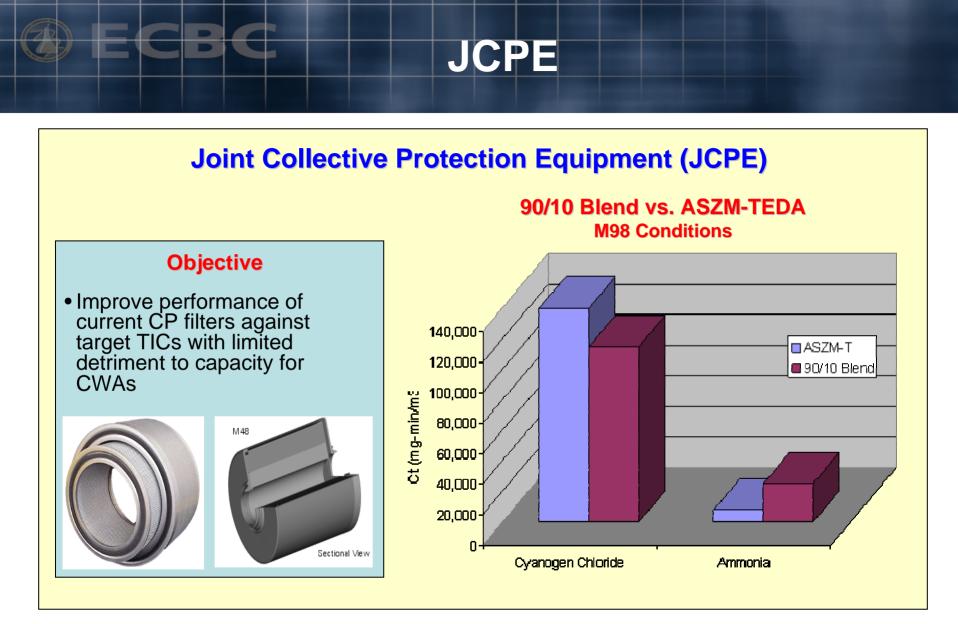
Radial Flow Filter - Inlet flow is directed to outer radial layer first and exits inner core, thus providing significant increase in chemical performance and reduction in airflow resistance



Split Flow Adsorber – Inlet flow is directed to center of two bifurcated cells, each containing particulate, CWA and TIC media

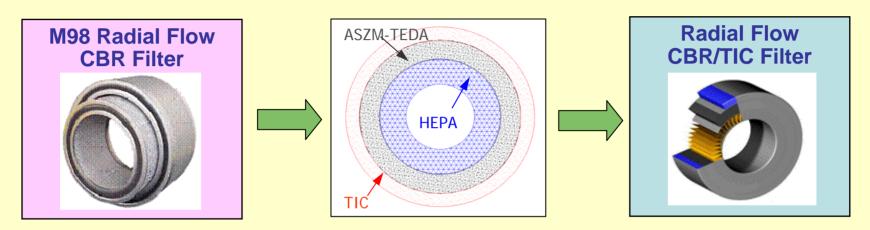
JSGPM





DARPA/NWA

DARPA/NWA CBR/TIC Filter

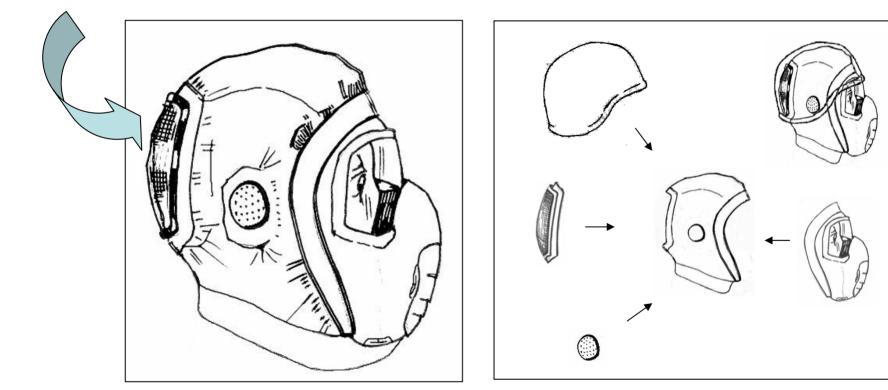


Objectives

- Provide ammonia, ethylene oxide and other TIC protection in addition to traditional CWA protection.
- Retrofit TIC protection into M98 filter housing.

ECB Concepts for Next Generation General Purpose Mask

Filter



Sorbent Bed Type

Packed Bed

- Maximum Sorption Activity
 per unit bulk volume
- Ideal for Higher Capacity Applications (>>50K CT)
- Constrained to Narrow Spectrum Chemical Protection
- Lower Unit Cost

Supported Bed

- Sorbent on Fiber Composite
- Ideal for Lower Capacity Applications (<50K CT)
- Suitable for Broad Spectrum
 Chemical Protection
- Suitable for Large Bed Area and Shallow Bed Configurations
- Higher Unit Cost

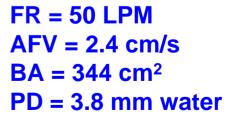
Effect of Filter Cross-Sectional Area on Performance

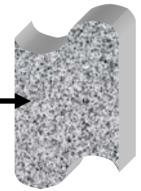


FR = 50 LPM AFV = 9.6 cm/s BA = 86 cm² PD = 15 mm water

Increasing Filter Area

- Reduced AFV
- Reduced PD
- •Reduced Particle Size
 - •Thinner Beds
 - Increased Chemical
 - Performance





FR = 50 LPM AFV = 4.8 cm/s BA = 172 cm² PD = 7.5 mm water

Effect of Particle Size on Mass Transfer Zone

Effect of Particle Size on MTZ

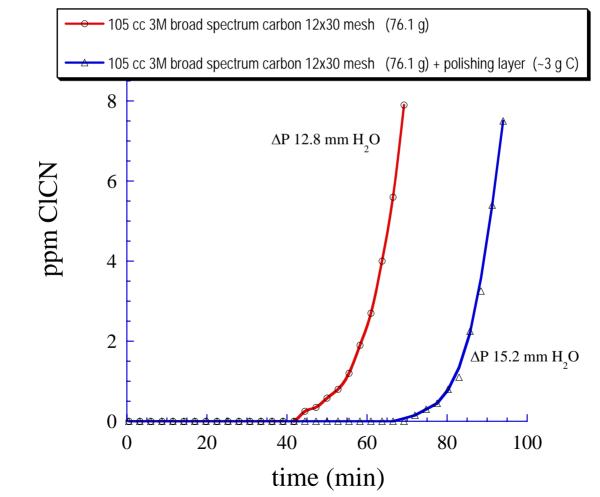
Pleated Axial Flow Bed ALC: NOT THE OWNER. 12x30 Effluent Conc. 20x40 **100 LPM** 60x150 External Area: 86 cm² AFV: <3 cm/s **Pleat Area: 600-900 cm2**

Time, min

Flex-c Web as CK Polishing Layer

550 ppm ClCN (1350 mg/m³) 32 L/min; 93% RH

loaded into 3M 6000 series cartridges ($\sim 67 \text{ cm}^2$)



Source: 3M

Summary

- For low capacity, broad spectrum protection (TIC/TIMs + CWAs) filter bed designs other than traditional packed bed sorbents may be necessary and advantageous to meet near-term and future requirements.
- **Supported Sorbents** offer a wide range of capabilities:
 - Composite thin beds with multiple sorbents
 - Suitable for non-conformal and pleated configurations
 - Smaller particle size sorbents
 - Lower airflow velocity and pressure drop
 - Flat sheet particulate media
 - Interchangeable beds and components

Summary

- Need for MATURING supported sorbent technologies
 - Supports
 - Gradual Increase in Sorbent Capability
 - Bed Design Concepts
 - Modeling
 - Compositions/Interchangeability
 - Manufacturability QA/QC
- Need funding opportunities to MATURE technology in order to equip the Warfighter in the near-term

Acknowledgements

- Corey Grove ECBC
- Greg Peterson ECBC
- Amy Maxwell -ECBC
- William Fritch ECBC, JPM-IP
- Britt Billingsly 3M Corporation
- Joseph Rossin Guild Associates
- Tom Van Doren New World Associates